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|--|---|----|-----|
| 14. State Wien's displacement Law.   | 2 | K1 | CO2 |
| 15. Compare natural and forced convection heat transfer.                                 | 2 | K2 | CO3 |
| 16. What is the difference between the local and average heat transfer coefficients?     | 2 | K1 | CO3 |
| 17. Interpret the differences between film wise condensation and drop wise condensation. | 2 | K2 | CO4 |
| 18. List out the applications of boiling and condensation process.                       | 2 | K1 | CO4 |
| 19. In a schematic show the flow configuration of cross flow heat exchanger.             | 2 | K2 | CO5 |
| 20. What are indirect contact heat exchangers?   | 2 | K1 | CO5 |
| 21. Differentiate between the heat transfer processes in boilers and condensers.         | 2 | K2 | CO6 |
| 22. Compare Counter flow and cross flow heat exchanger.                                  | 2 | K2 | CO6 |

**PART - C (6 × 11 = 66 Marks)**

Answer ALL Questions

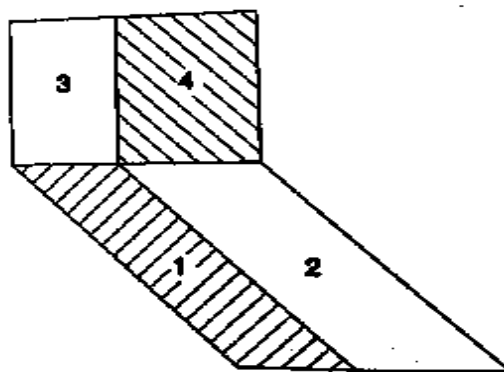
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|--------|--|----|----|-----|
| 23. a) | A composite wall is formed of a 2.5 cm copper plate ( $k = 355 \text{ W/mK}$ ), a 3.2 mm layer of asbestos ( $k = 0.110 \text{ W/mK}$ ) and a 5 cm layer of fibre plate ( $k = 0.049 \text{ W/m.K}$ ). The wall is subjected to an overall temperature difference of $560^\circ\text{C}$ ( $560^\circ\text{C}$ on the Cu plate side and $0^\circ\text{C}$ on the fibre plate side). Estimate the heat flux through this composite wall and the interface temperature between asbestos and fibre plate. | 11 | K3 | CO1 |
|--------|--|----|----|-----|

**OR**

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| b)     | A steam pipe 10 cm I.D and 11 cm O.D is covered with an insulating substance ( $k = 1 \text{ W/mK}$ ). The steam temperature and the ambient temperatures are $200^\circ\text{C}$ and $20^\circ\text{C}$ respectively. If the convective heat transfer coefficient between the insulating surface and the air is $8 \text{ W/m}^2\text{K}$ , find the critical radius of insulation. For this value of $r_o$ (outer Radii), Estimate the heat loss per meter length of pipe and outer surface temperature. Neglect the resistance of pipe material. | 11 | K3 | CO1 |
| 24. a) | A gray surface is maintained at a temperature of $900^\circ\text{C}$ and maximum emissive power at that temperature is $1.4 \times 10^{10} \text{ W/m}^2$ . Calculate the emissivity of the body and the wave length corresponding to the maximum intensity of radiation.   | 11 | K3 | CO2 |

**OR**

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|----|--|----|----|-----|
| b) | Find the shape factor, $F_{14}$ , by shape factor algebra for rectangles perpendicular to each other but not in line (as shown in Fig.): | 11 | K3 | CO2 |
|----|--|----|----|-----|



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|--------|---|----|----|-----|
| 25. a) | Air at $25^\circ\text{C}$ , flows over a flat plate at a velocity of $5 \text{ m/s}$ and heated to $135^\circ\text{C}$ . The plate is $3 \text{ m}$ long and $1.5 \text{ m}$ wide. Calculate the local heat transfer coefficient at $x = 0.5 \text{ m}$ and the heat transferred from the first $0.5 \text{ m}$ of the plate. | 11 | K3 | CO3 |
|--------|---|----|----|-----|

**OR**

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|----|--|----|----|-----|
| b) | Water at $50^\circ\text{C}$ flows through an automobile radiator tube $0.5 \text{ cm}$ inner diameter, $50 \text{ cm}$ long with a mean velocity of $1 \text{ m/s}$ . The surface of the radiator tube is at $30^\circ\text{C}$ . Determine the heat transfer coefficient using Colburn analogy. | 11 | K3 | CO3 |
|----|--|----|----|-----|

26. a) A nickel wire carrying electric current of 1.5 mm diameter and 50 cm long, is submerged in a water bath which is open to atmospheric pressure. Find the voltage at the burn out point, if at this point the wire carries a current of 200A. 11 K2 CO4

**OR**

- b) Dry saturated steam at a pressure of 2.45 bar condenses on the surface of a vertical tube of height 1m. The tube surface temperature is kept at 117°C. Find the thickness of the condensate film and the local heat transfer coefficient at a distance of 0.2 m from the upper end of the tube. 11 K2 CO4
27. a) In a counter flow heat exchanger; oil is cooled from 85°C to 55°C by water entering at 25°C. The mass flow rate of oil is 9800 kg/h and specific heat of oil is 2000 J/kg K. The mass flow rate of water is 8000 kg/h and specific heat of water is 4180 J/kg K. Determine the heat exchanger area and heat transfer rate for an overall heat transfer coefficient of 280W/m<sup>2</sup>K. 11 K3 CO5

**OR**

- b) In a parallel flow heat exchanger, hot liquid enters at 400°C and leaves at 250°C. Cold fluid enters at 50°C and leaves at 110°C. The inside and outside heat transfer coefficients are 120W/m<sup>2</sup>K and 190W/m<sup>2</sup>K respectively. Inside and outside diameters of the tube are 0.06m and 0.08m respectively. If the heat transferred per hour is 1.6x10<sup>5</sup> kJ, find the length of the tube required. 11 K3 CO5
28. a) Saturated steam at 120°C is condensing on the outer surface of a single pass heat exchanger. The heat transfer coefficient is  $U_o = 1800 \text{ W/m}^2\text{K}$ . Determine the surface area of the heat exchanger capable of heating 1000 kg/h of water from 20°C to 90°C. Also compute the rate of condensation of steam. Take  $h_{fg} = 2200 \text{ kJ/kg}$ . 11 K3 CO6

**OR**

- b) In a counter flow heat exchanger, water at 20°C flowing at the rate of 1200 kg/hr. It is heated by oil of specific heat 2100 J/kgK flowing at the rate of 520 kg/h at inlet temperature of 95°C. Determine the Heat transfer, outlet temperature of water and oil. Take Heat exchanger area as 1m<sup>2</sup> and overall heat transfer coefficient as 1000 W/m<sup>2</sup>K. 11 K3 CO6

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